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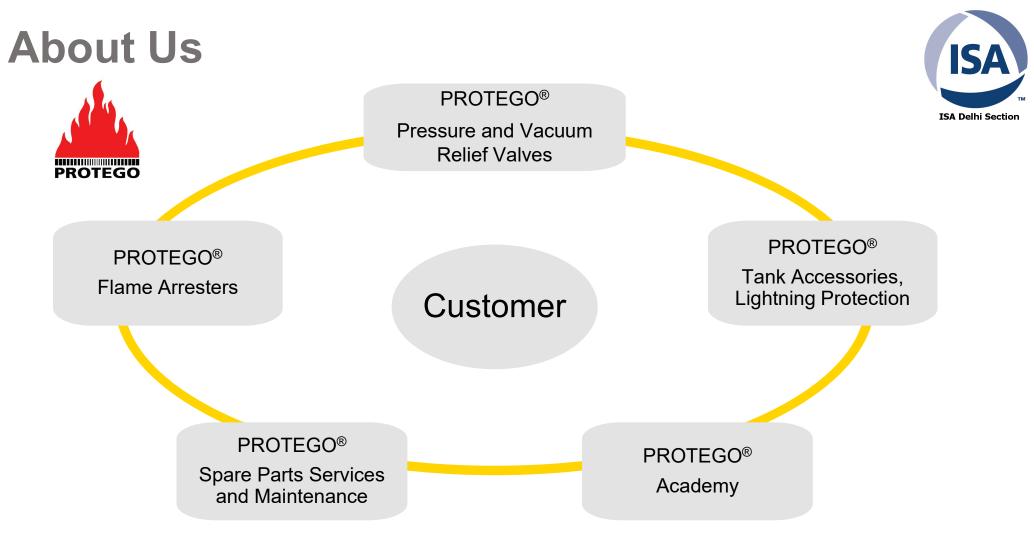
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Safety Solutions for Cryogenic Storage Tanks

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Safety Solutions for Cryogenic Storage Tank

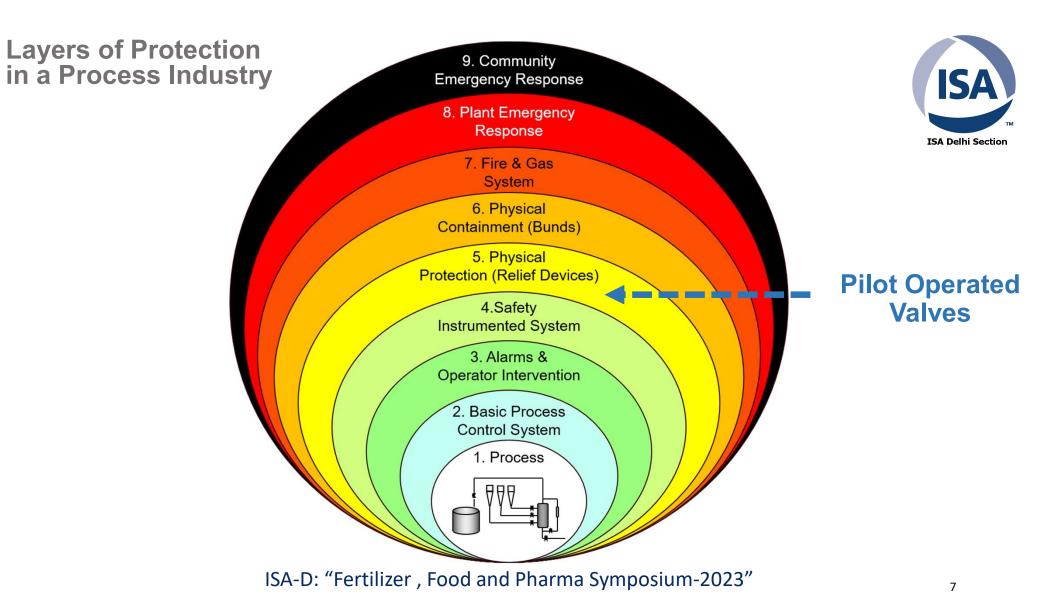


- 1 Lessons learnt solving Pilot Valve Instability Issues
- 2 Emergency Shutdown using In Tank Valve



2 Emergency Shutdown using In Tank Valve







Key Definitions

Pilot operated safety valve

Safety valve, the operation of which is initiated and controlled by the fluid discharged from a pilot valve which in itself is a direct loaded safety valve subject to the requirement of this standard (DIN EN ISO 4126-1 2004)

Types of pilot operated valves

Modulating

Action is characterised by a gradual opening and closing of the disc of the main valve which is a function of the pressure, proportional but not necessarily linear (DIN EN ISO 4126-4 2004)

ON/OFF (a.k.a. as POP-Action)

Action characterised by stable operating resulting in fully open or fully closed main valve position. (DIN EN ISO 4126-4 2004)





- In accordance with API 2000 recommendations
- Set pressure up to 1034 mbar and -7 mbar
- Blow Down < 7%
- Optimized flow performance
- The valve can be put to service in applications where temperatures as low as –196°C prevail.
- Variants:
 - Spring-loaded pilot valve
 - Magnet pilot valve













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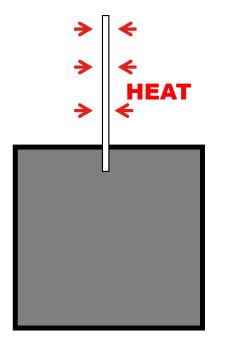


Observations:

- Common guidance on how to design the piping seems to be missing or is not applied in all cases
- Inlet pressure loss seems to be neglected in some cases
- Built up pressure in the discharge line is not allways considered

• The tank is insulated but the discharge pipeline may not be





- In the discharge line the cryogenic gas warms up due to heat input from environment
- Consider the density changes along the line when calculating the pressure losses and the tank relief loads
- Build up your own or use a commercial package with a reliable thermo-fluid dynamic model
- Consider the internal piping within the tank



- Pilot operated pressure relief valves installed on storage tanks may become unstable as a result of inaccurate plant / Pilot Valve design / selection or sudden construction changes on site, which may result into extensive cost increments and delays in the start-up of new storage facilities.
- Pilot operated valves which are forced to become unstable may not provide sufficient relieve capacity resulting in overpressure and imposing safety risks to the facility.
- It is known that relief value instability is a dynamic problem which requires an understanding and coupling of the pressure source (e.g. storage tank), the inlet line, the pilot operated pressure relief value and the discharge line

Challenge:

Start up with small vaporizing quantaties can result in valve instability





Types of Instability

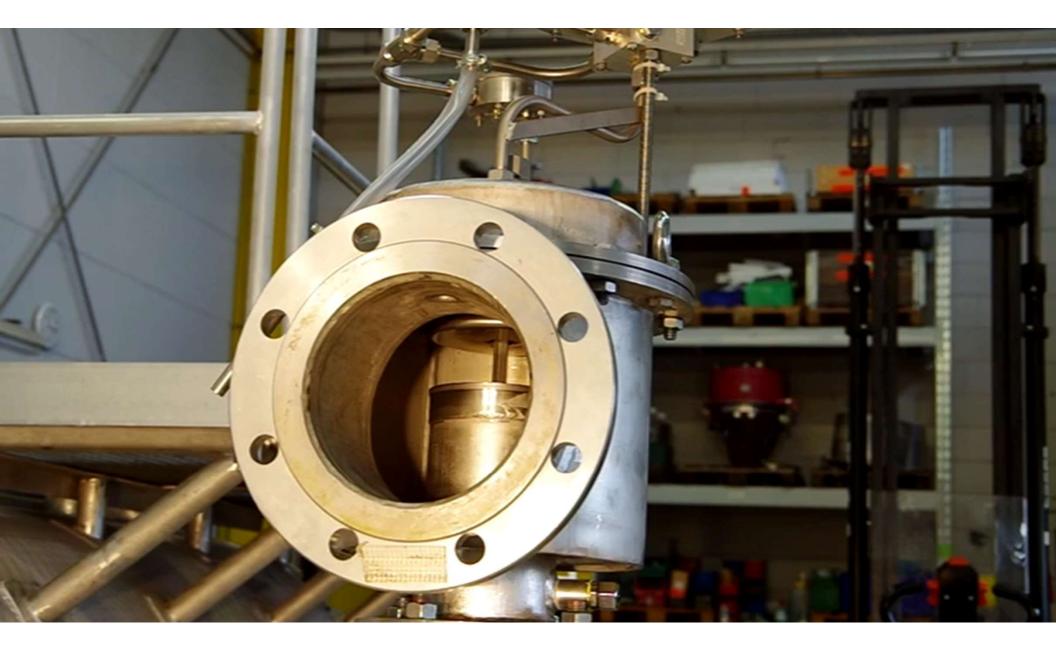
- **Cycling** : The least dangerous level of instability and it typically occurs, when the required flow rate is a fraction of the capacity of the fully-opened device. As for all oscillatory phenomena safety and relief valve cycling has a low frequency of the order of magnitude of one cycle per second.
- **Fluttering** : In a fluttering valve the moving parts oscillate abnormally rapidly with a frequency of the order of magnitude of their natural frequency. Rapid wear of the moving parts and the eventuality of a non-reclosing valve when the moving parts get stuck are common failures for fluttering valves.
- **Chattering**: In the worst case scenario of a fluttering valve, where the moving parts hit the seat, the valve is said to chatter. The primary concern for chattering is the loss of product, for instance due to loosening of flanges; as well as seat damage or adhesive wear and bellows rupture. There are examples in which chattering destroyed the valve pallet completely.

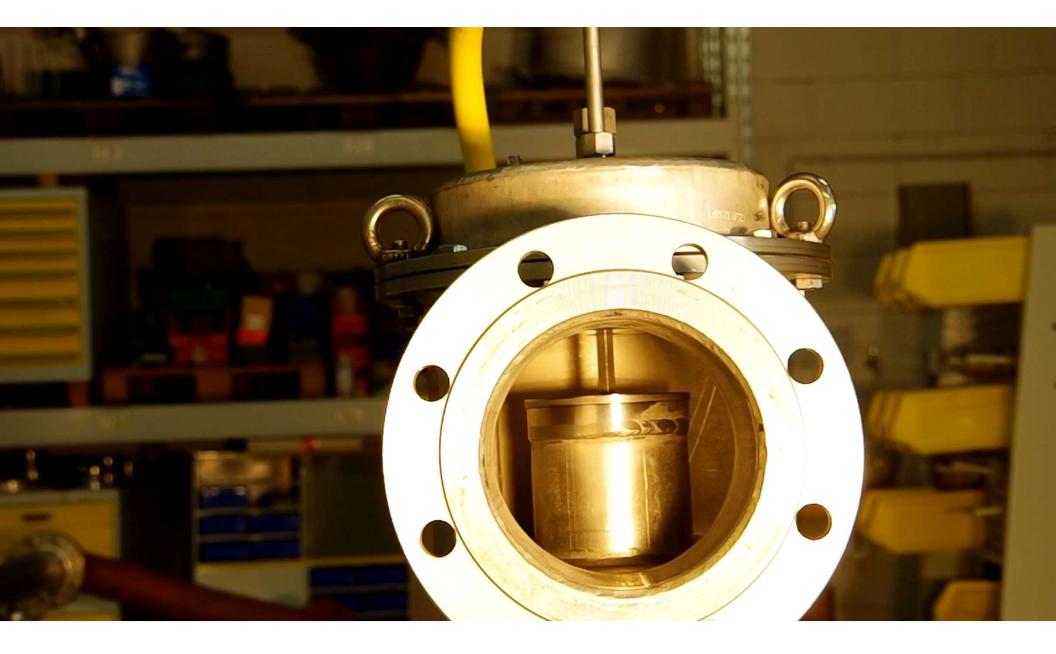




Solution:

Dampening systems can prevent valve instabilty

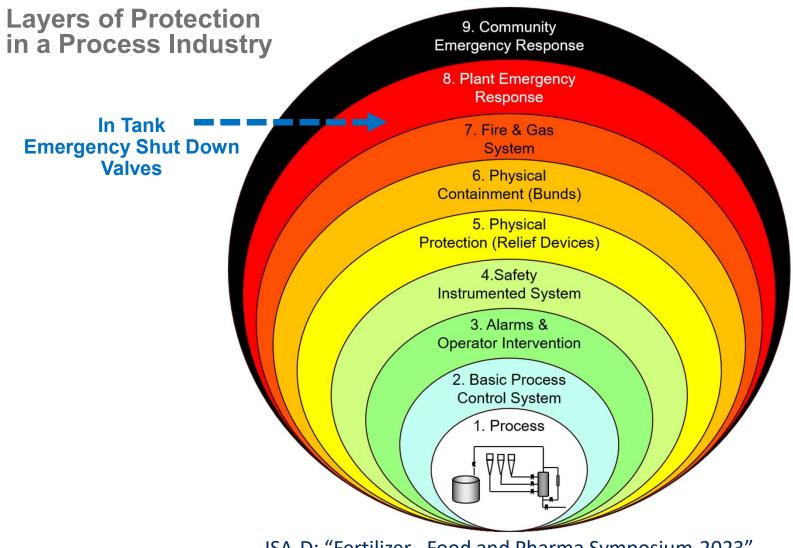






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API Standard 625 ; Tank Systems for Refrigerated Liquified Gas Storage

5.5 Double or Full Containment-with-Penetrations Tank System

d) In-Tank Valves are provided (refer to 7.3.1.4.2 b);

7.3.1.4.2: specific requirements for single containment tank systems

b) In-Tank Valves shall be considered when bottom or shell process lines are used. The In-Tank Valve shall be automatically activated due to failure of external piping and shall also be automatically activated during a loss of electrical power and shall be capable of being activated from a remote location. The design and installation of an In-Tank Valve shall be such that any failure of the penetrating nozzle resulting from external pipe strain is beyond the shutoff seats of the internal valve itself.

Reasons for triggering an In-Tank Valve:

- Failure of compressed air
- Failure of power
- Failure of the pipe strain outside the tank recognized, detection by vapor observation cameras, pressure or flow control sensors
- Manually activated
- Activated from the control room/ remote location





PROTEGO® ITV-S-250-250



PROTEGO® ITV-S-400-350

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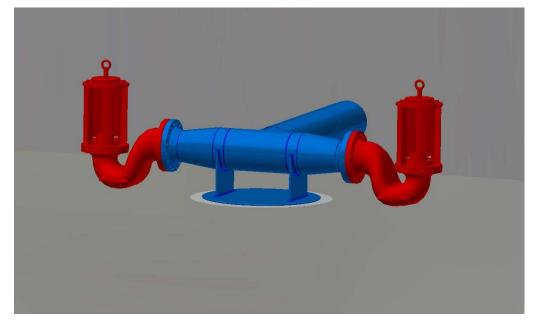












Key Safety Features



- 1. Shuts Down within 10 seconds.
- 2. Actuation failure due to Power or Pneumatic failures do not interfere with valve closure.
- 3. Stops the product loss within 10 second to mitigate the risk of secondary accident and damages.
- 4. No repair and maintenance required as no soft sealing.
- 5. Various installation combinations possible.

General Design Requirements

- 1. Light weight design and No forces or stress into the tank bottom.
- 2. Slim design creating no dead volume.
- 3. No requirement for guidance on the tank bottom.
- 4. No impact due to tank bottom movement or shrinkage or elephant foot.
- 5. Maintenance free over the life time of the tank or at least 30 years.
- 6. In-tank valve should be able to work with dirt particles due to Ni-steels which are absorbing rust particles.



General Design Requirements

- 10. Minimize the reaction force when the valve closes.
- 11. Reaction time /closing time when activated.
- 12. Factor 10 in the design as safety margin rope / chain.
- 13. Mis-alignment between valve and actuator of 3° should be be no problem
- 14. Actuator need to be sealed against the tank vapour head.





