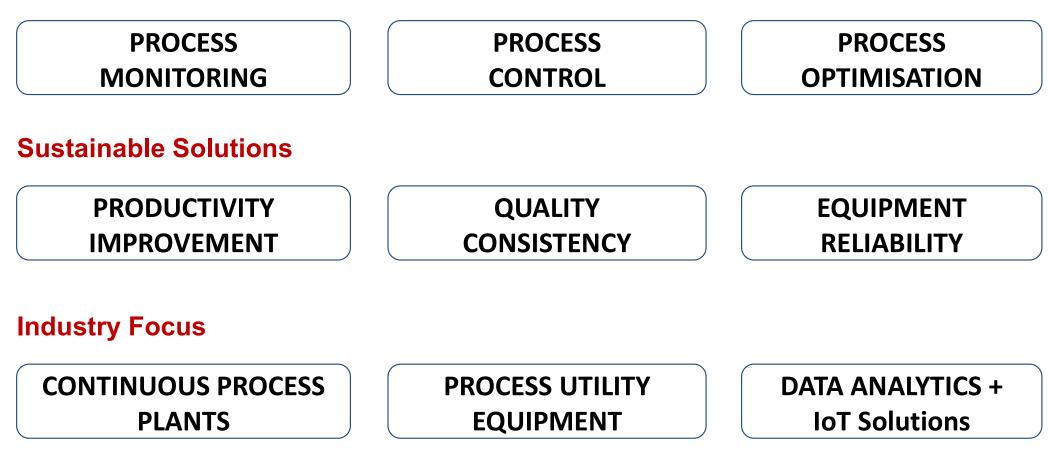


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Products + Services



Overview Presentation : Fertilizer, Pharmaceutical and Food Industry case studies November, 2022



(Innovative Product)

(DIPP 2649)

(I.I.T. Madras)

(30+ Yrs of Engg Service)



OPTIMIZING

Harnessing Data >> Extracting Knowledge >> Creating Value

Products / Services / Projects for improving

Process Performance, Quality Consistency, Equipment Uptime Plant Productivity, Energy Efficiency, Safety and Environmental Parameters

 Mill Operation • PID Tuning Process Variability Multivariate Control • Fuel Efficiency Controller Performance • Feed Forward Logic Cooler Recuperation • Equipment Health Smart Combustion Control • Quality Consistency • Sensor Analysis Supervisory control MONITORING

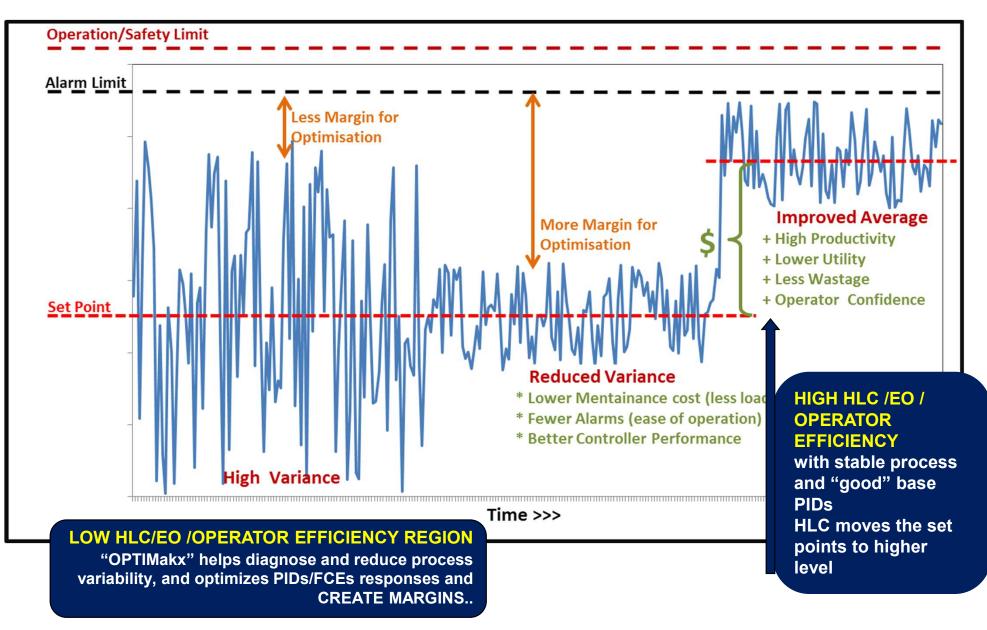
CONTROLING



High Variance >> Inconsistent KPI >> Less confidence/margin for Improvement

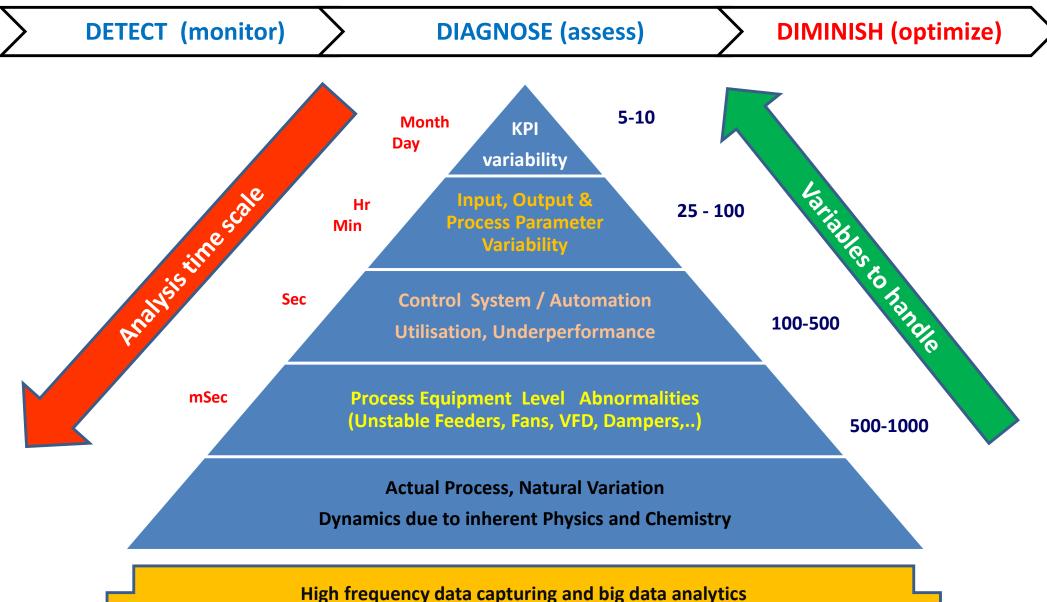
REDUCE fluctuations >> IMPROVE variance >> OPTIMIZE averages

>> OPTIMakx adds to STABILITY (low variability) and CREATS MARGINS for EO





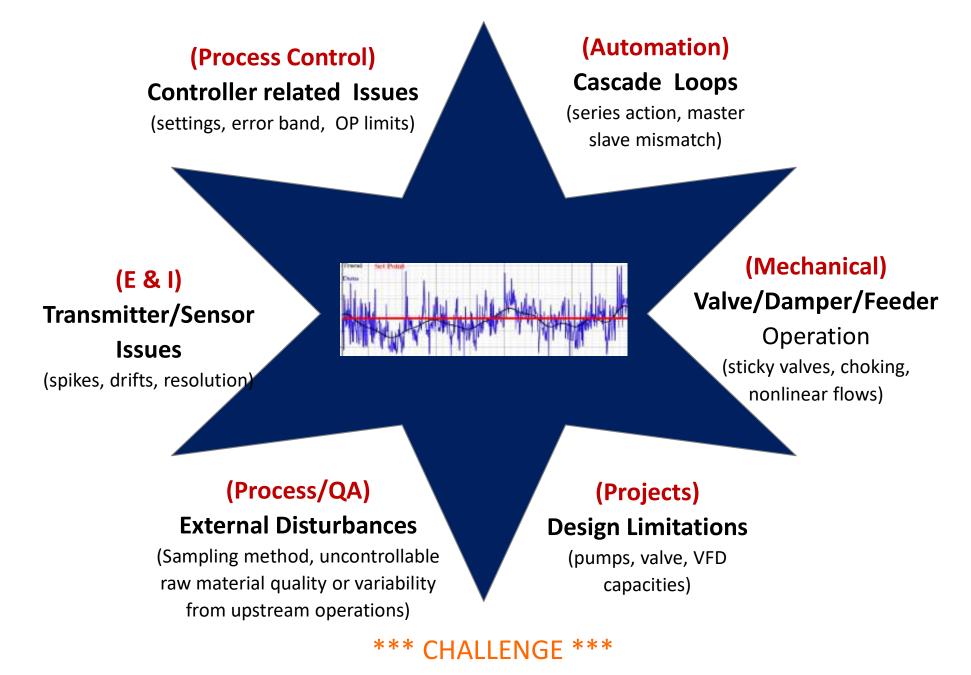
APPROACH :: PLANT WIDE FLUCTUATION MAPPING



Benchmarking/Detection/Diagnosis/Impact Analysis using AI/ML algorithms

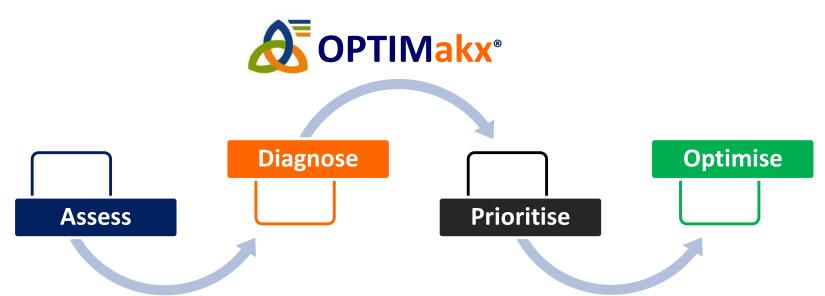


Process Plant Fluctuations :: Sources we chase..



How to identify, quantify & resolve these in a large/continuous plant.





>> Suite of AI and Statistical Algorithms, researched and developed at IIT Madras.
 >> Open Source IT plat form, Web Based Application for IoT and Industry 4.0 needs.
 >> Automatic assessment, diagnosis and decision support for continuous improvement
 >> Multi plant, Multi process, Multi user configuration for remote monitoring/benchmarking

- >> 20+ different scientific/statistical measures for performance benchmarking.
- >> 15+ different root causes diagnosed for abnormal operation/high fluctuations.
- >> **500+** variables simultaneously tagged, tracked, issues diagnosed, compared.
- >> Visuals, Work Flow Annotation, Alarms and Auto Reporting, SuperAdmin features.



Services and Automated Decision Support Tools for

Productivity Optimisation, Energy Efficiency Enhancement and Quality Consistency

CEMENT, MINERAL & METAL PROCESSING



FERTILIZER & PESTICIDE, PHARMA



PULP PROCESSING & PAPER / BOARDS



GLASS & CERAMICS



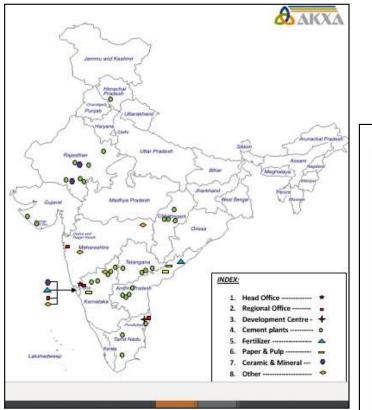
POWER PLANTS CAPTIVE / CO-GEN



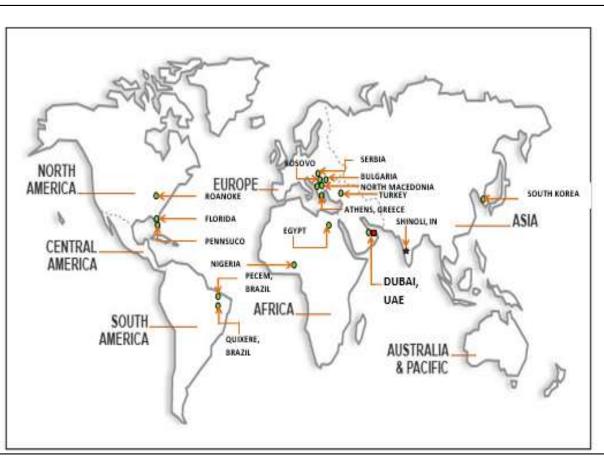
ANY CONTINUOUS PROCESS PLANT







- TEN CORE SECTORS
- 160+ plants in INDIA / Global
- International Projects, Nine Countries



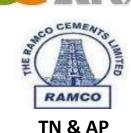


Range of Process Industries (Services Offered)





Prestigious Clients (CEMENT) – in last **TWO YEARS..**





ALL 5 Plants –TS / AP



17 plants (Europe/Americas)





UAE





12 plants



40 plants





Dalmia cement FUTURE TODAY













Kurnool (AP)



Kalburgi

Cement





ENGINEERING THE FUTURE



... with the support and inputs from innovative Technology & continuous service offered by team-AKXA ...

Our clients have improved the Productivity & Energy Efficiency of various equipment of their plants

CASE STUDIES

THE RESULT OF AKXA INTERVENTION ON EXISTING OPTIMIZED PROCESSES

-using the OPTIMakx suite of Decision Support Tools-

Benefits leading to Total Savings

with Pay Back Period of LESS THAN ONE YEAR on Investment / Fees.



NPK FERTILIZER SECTOR SCOPE OF SERVICES

Process Fluctuation Assessment

-- NPK product quality data assessment (Different Grades)

-- Fluctuation Source Assessment (Flow / Sampling / Valve / Instrument / Controller issues)

AUTO Sampler : automated, composite sampling.

-- Fully automated AUTO SAMPLER – customized design (Chute and Belt Type)

-- Reduces sampling related quality variation by over 50%.

Controller Performance Diagnosis and Optimisation

-- Control System performance assessment / diagnosis and Optimization

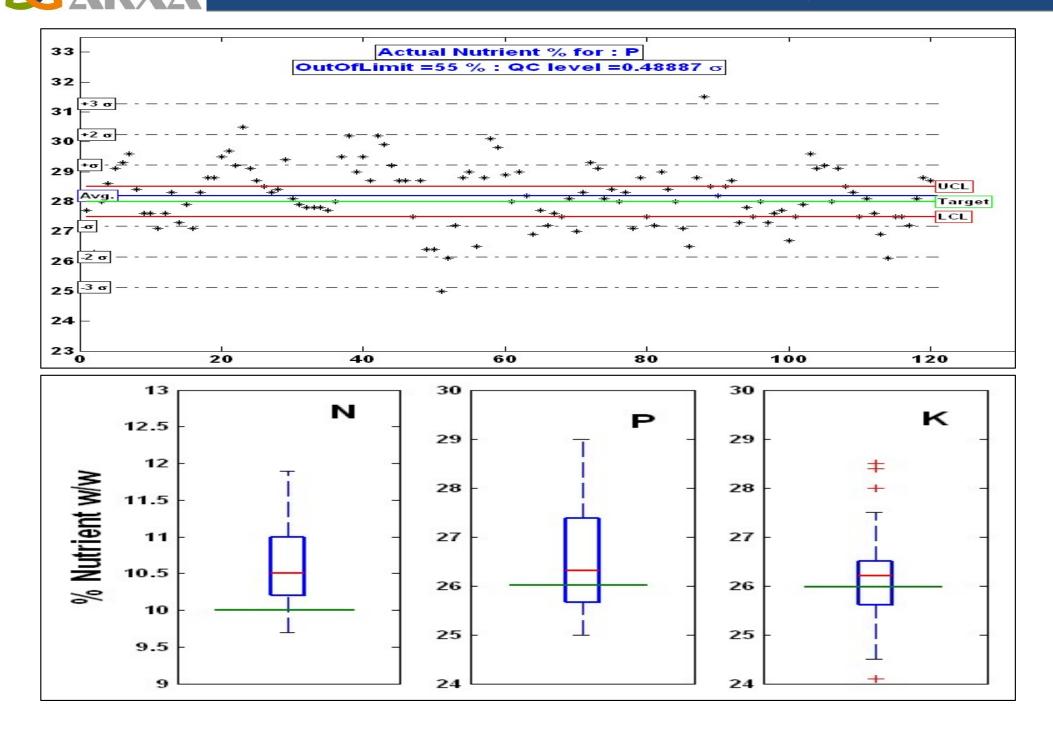
NPK Nutrient Prediction Model (both off line and online version)

-- Steady State /
Dynamic material
balance model - Fine
tuned to site
conditions.
30 to 45 minutes
ahead prediction of
NPK nutrient % (8090% accuracy)
-- Generalizable to
different grades in
single plant.

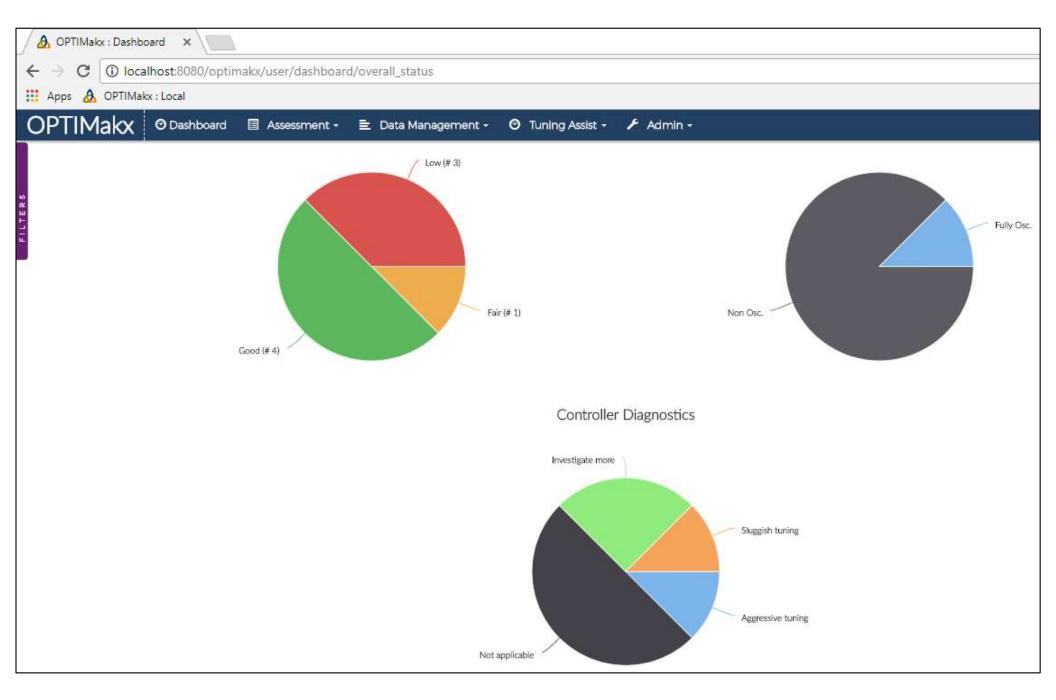


		BEFORE				AFTER			
TAG	Description	Avg.	Std. Dev.	% Variability		Avg.	Std. Dev.	% Variability	
xxxPICx0xB	PN NH3 PRESSURE	10.4	1.1	10.5		10.3	1.0	9.7	
xxxFlCx4xB	PN NH3 FLOW	5.1	0.7	13.7		5.0	0.5	10	
xxxPICx06B	GRAN NH3 PRESSURE	12.6	1.2	9.5		12.2	0.8	6.5	
xxxFICx48A	GRAN NH3 FLOW	1.4	0.1	7.1		1.4	0.06	4.2	
xxxFICx63	PN 48%	201.7	26.5	13.1		202.0	17.9	8.8	
xxxFICx63B	PreScrubber 48%	40.7	5.2	12.7		40	3.7	9.25	
xxxFICx42	H2SO4	5.0	1.3	26		5.0	0.4	8	
xxxFICx42A	PS H2SO4	11.8	2.8	23.7		11.0	1.2	10.9	
xxxWICx21	WEST FEEDER	17.7	1.9	10.7		18	0.95	5.3	
Failu	Failure Rates			42%)	Low (<20.2%)			.2%)	

Statistical Control Chart & Variance Analysis : VISIBILITY







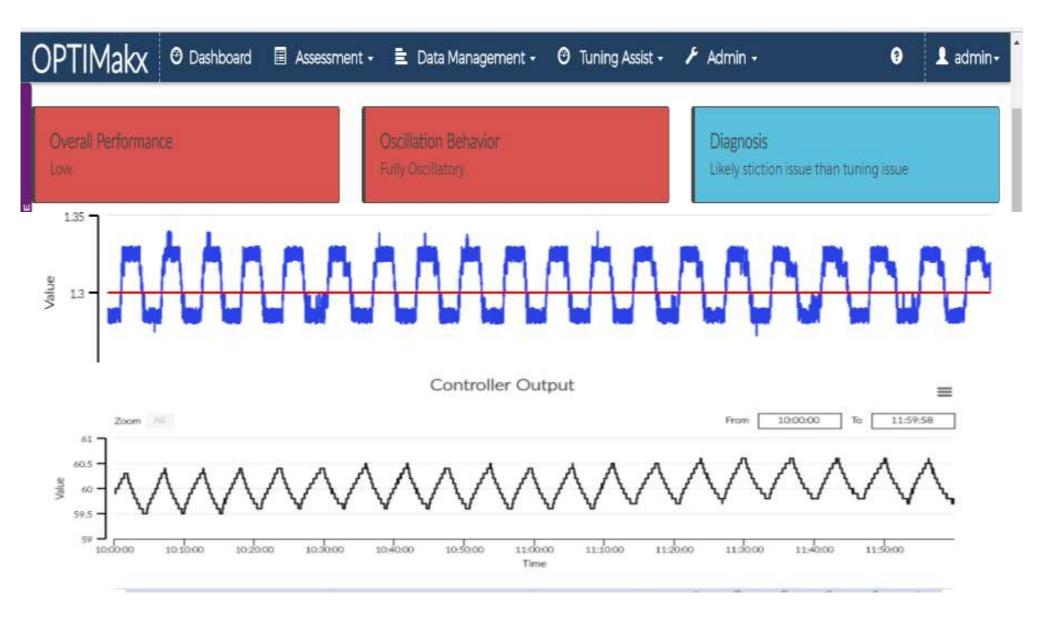


Sluggish Tuning Detected in Flow PID loop



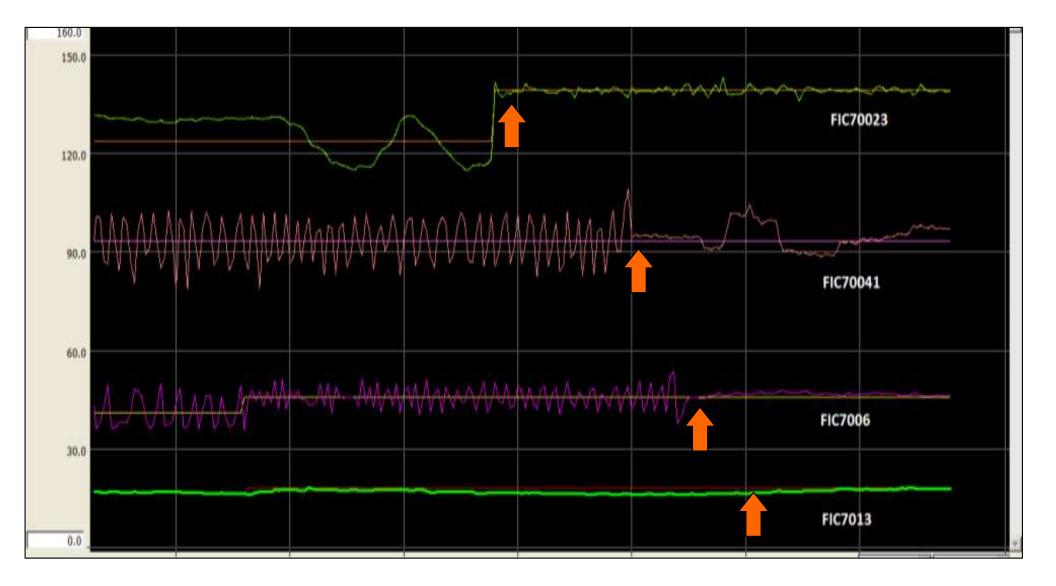


Actuator Valve related issues highlighted (predictive maintenance)





Continuous oscillations eliminated. OFFSET removed. Process Stabilized





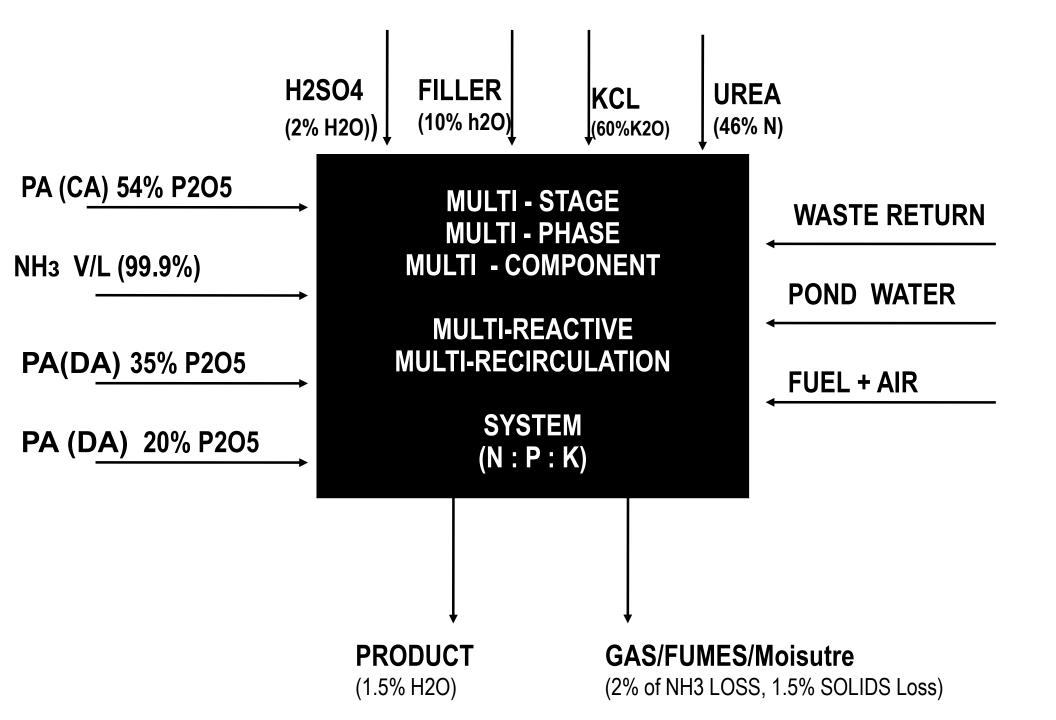
Belt Conveyer (Horizontal or Inclided) based AUTO sampler

- >> Compressed air (4 to 6 kg) operated sampler
- >> Automatically draws samples at fixed intervals Swipes across Belt
- >> Customized to fit into existing site.
- >> Flexible levers for height, scoop length and angle adjustment.
- >> Elastic scooper tip does not damage the belt even during belt sways.

(located at cooler outlet or product belt conveyor sampling points)





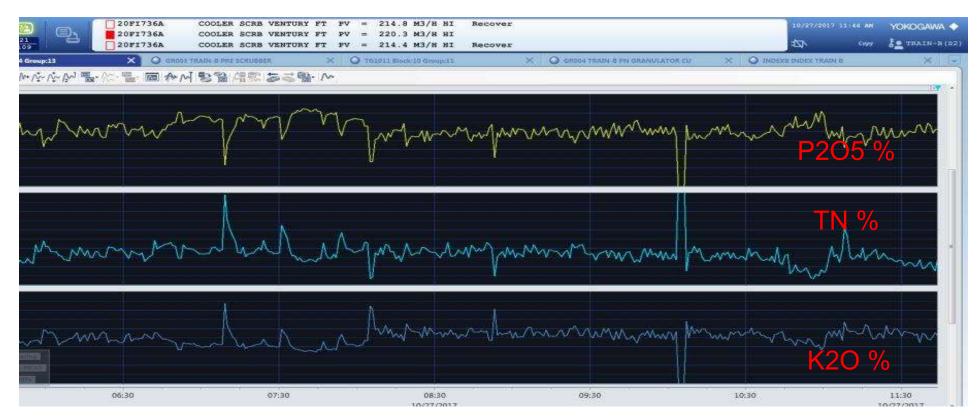




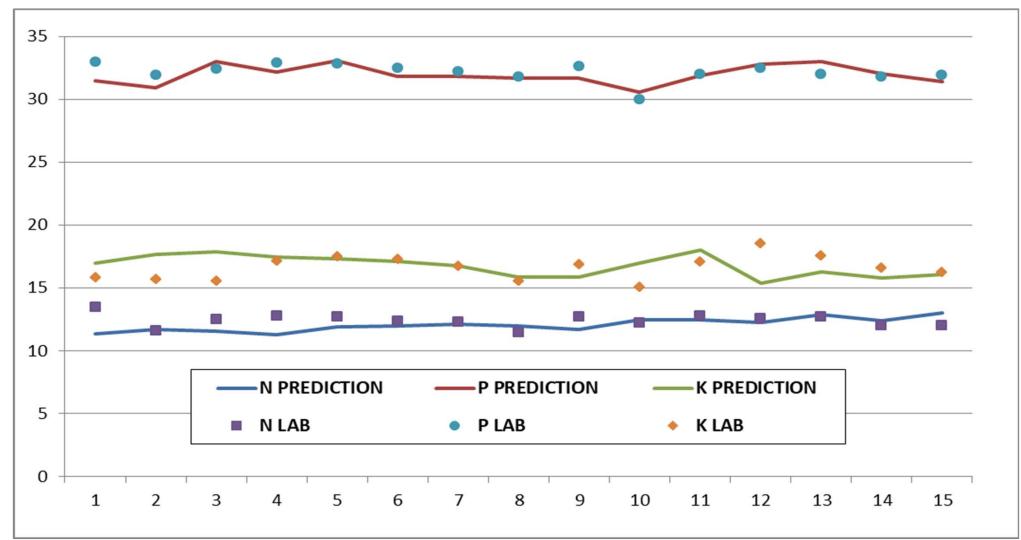
NPK Predict :: ONLINE Model as implemented in B train

NOVING AVERAGES	CALCULATIONS
N. 2010 No. 2010	24 PHD_AM_CH222 [PHD_IM_CH224 PHD_IM_CH2 24 PHD_IM_CH224 PHD_IM_CH24 24 PHD_IM_CH2 ADD PHD_CH2 CALCOT
NAMULE HITEY 0_140_000 00_44_200 20_72000_00 0_72100_00 NLD NLD NLD NLD NLD 0_240_000 ND_2000 0_72100_00 0_72100_00 0_72100_00 NLD NLD NLD NLD NLD NLD VLO NLD NLD NLD NLD NLD NLD	DCS model block

Model Prediction Trends







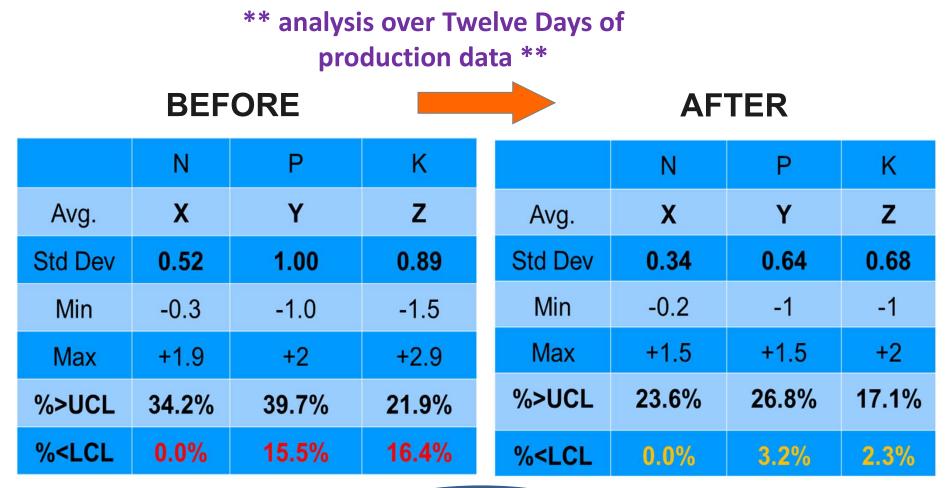
NPK Predict Overall Result

N% prediction :: 94.5% P% prediction :: 97.4% K% prediction :: 94.2%



>> Nutrient (Product Quality) fluctuations.

>> Actions : Nutrient Prediction Model, Auto Sampler, Input Flow controller Tuning



15 - 20% Lower Rejection



Ammonia and Urea Plant: Plant Wide Fluctuation Assessment and Root Cause Analysis

- 1. KPI variability assessment for Ammonia and Urea Plant. (Production, NG Conumption, Steam, Power and Energy consumption).and Quality parameter variability assessment
- 2. Process Variables data variability Assessment (Input variables, Inprocess variables and Output variables from each section of the Ammonia and Urea plant almost up to 500 Process Variables).
- 3. Controller Performance Evaluation for all types of situations (Disturbance, Rejection, Set Point Change . .) to be analysed. (almost up to 200 control loops in typical Ammonia and Urea Plant) and Diagnosis for underperforming control systems and establishing reasons for the same.
- 4. Benchmarking of Fluctuation and their impact on KPIs (Energy Efficiency and Productivity.)
- 5. Potential to Implement new Feed forward logics and development of Soft sensors to be Evaluated.
- 6. Establishing overall scope for reduction in "Plant Wide Process Fluctuations" and Potential IMPROVEMENT in the performance of High Level Controller (APC).

Harnessing Data , Creating Value

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Overall Variability Heat Map

	1	Р	0	
NG PREHEATER	60	25	15	
Final Desulphurisation Section	-	25	10	
Primary Reforming Section	50	70	10	0 - 20 Stability
Secondary Reforming & Steam Drum	75	45	30	20 - 40
CO Shift Conversion	15	10	25	40 - 60
CO2 Removal Section	40	50	75	60 - 80
Methanation Section	80	65	10	80 - 100 Unstability
Synthesis Section	65	30	85	
DM Water & Steam Condensate	70	90	-	
Steam Circuit	15	-	70	 No Variables categorized
Process Air & Instrument Air	10	-	-	
				-

- Input Variations : Some of the input variables like NG fuel and NG process gas , Process air, Combustion Air, Steam and Recycle gases shows abnormal oscillations they could be due to Cascade effects and Abnormal controller behaviour or continuous disturbance from the APC >> These input variations to be studied and Root cause for that to be established.
- Inprocess Variations : Inprocess Variables (such as Primary Reformer Combustion Air Temperatures, Excess Oxygen,H2/N2 Ratio, Primary Reformer Collector Temperature 2, Reforming Temperature, Methanator Temperature, WHB level etc >> Further investigation of the controllers required.
- Output Variations : Once Input and Inprocess variations stabilised then automatically these output variations will be controlled.

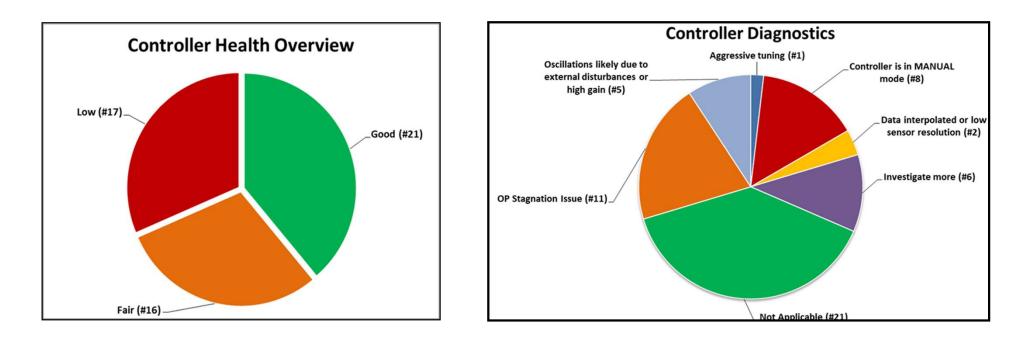


OVERALL Base Case Performance Assessed and Classified using OPTIMakxCORP [®] Classification based on average controller error%.

GOOD – working well in AUTO, FAIR – Need more observation, POOR – SubOptimal (scope for improvement)

OPTIMakx PID performance : Overall

Total 54 loops = 21 in Good + 16 in Fair + 17 in Low performance (Scope for Improvement)



- > Nearly 39% of the loops are stable and need no intervention
- 30% loops needs observation and action
- **Remaining 31% (17 loops) are underperforming with scope for improvement.**



Overall Variability Heat Map

	I.	Ρ	0	
Synthesis Section 1 and 2	70	25	10	0 - 20 Stability
First and Second Stage Rectifying Section	65	85	15	20 - 40
Vaccum and Crystallisation section	20	70	-	<mark>40 - 60</mark>
Prilling Section	60	75	25	60 - 80
Utility Section	-	85	10	80 - 100 Unstability
Hydrolyser Stripper Section	15	65	25	
	- No Variables categorized			

- Input Variations : Some of the input variables (Ammonia inlet flow, preheater temp,CO2 from regenerator,CCP ******main pump discharge pressure, CCP suction flow and Steam pressure inlet to Remelter heater) shows abnormal oscillations they could be due to Cascade effects and Abnormal controller behaviour >> These input variations to be studied and Root cause for that to be established.
- Inprocess Variations : Inprocess Variables (such as Reactor B bottom temperature, Ammonia Scrubber inlet <u>م</u> temperature, Reflux condenser level tank outlet temperature, Evaporator heater level, Urea Solution pump discharge, Prilling Tower) >> Further investigation of the controllers required
- **Output Variations :** Once Input and Inprocess variations stabilised then automatically these output variations <u>م</u> will be controlled.

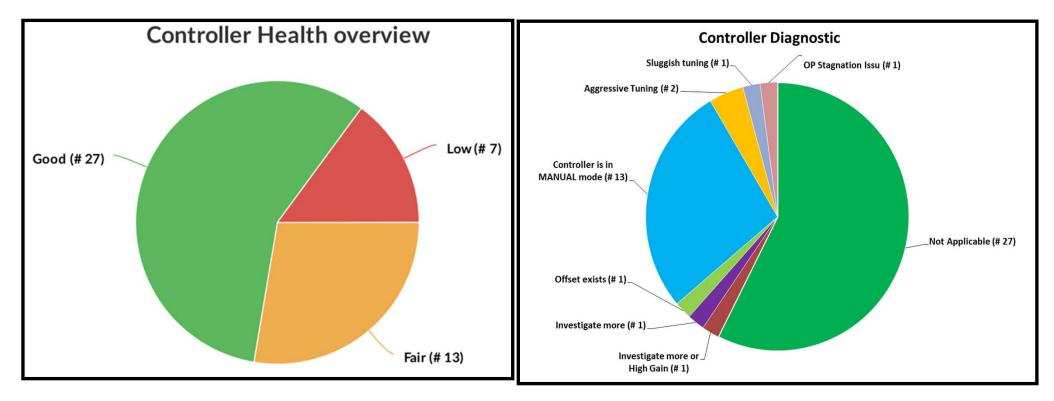


OVERALL Base Case Performance Assessed and Classified using OPTIMakxCORP [®] Classification based on average controller error%.

GOOD – working well in AUTO, FAIR – Need more observation, POOR – SubOptimal (scope for improvement)

OPTIMakx PID performance : Overall

Total 47 loops = 27 in Good + 13 in Fair + 7 in Low performance (Scope for Improvement)



- Nearly 58 % of the loops are stable and need no intervention
- 28% loops needs observation and action
- Remaining 14% (7 loops) are underperforming with scope for improvement.



Pharmaceutical Plant: Plant Wide Fluctuation Assessment and Root Cause Analysis

- **PID Optimization** for Temp/Flow/RH /pH/Ozone control @ Coating Machines, FBDs, Packing m/cs, WTP
- AHU : performance review, detecting limitations, optimizing responses
- **VFD optimization** for major drives on blowers, compressors and fans
- □ Valve diagnostics: Nonlinearity assessment of all process and actuator valves
- □ Assessment and diagnosis of rejection/quality inconsistency data.

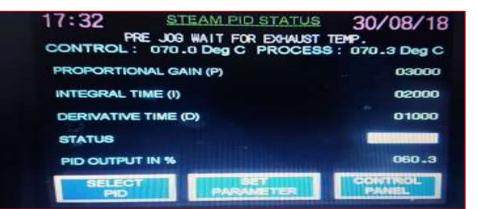
Harnessing Data, Creating Value

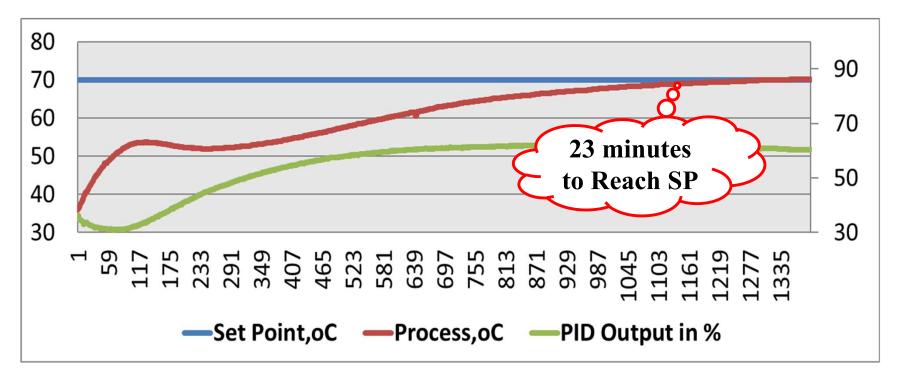
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Coating Machines : DigitEyes tool Video to Data conversion

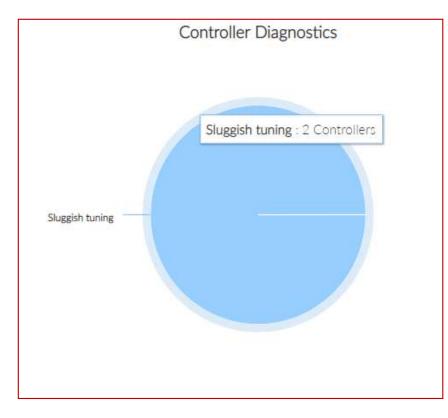
TEMPERATURE PARAMETERS	SET	PROCESS
NLET AIR TEMP. Deg C	070.0	070.2
EXHAUST AIR TEMP. Deg C	053.3	051.8
SOLUTION TANK HEATER Deg C	020.0	255.0
SPEED PARAMETERS	SET	PROCESS
NLET BLOWER SPEED IN RPM	1500	1500
EXHST BLOWER SPEED IN RPM	1100	1100
PAN MOTOR SPEED IN RPM	00.0	00.0
DOSING PUMP SPEED IN RPM	004.0	0.000





Temperature Control loop	AUTO
Absolute Control Error %	19.74





Assessment clearly showed that both the loops have higher controller error during Start-up cycle.

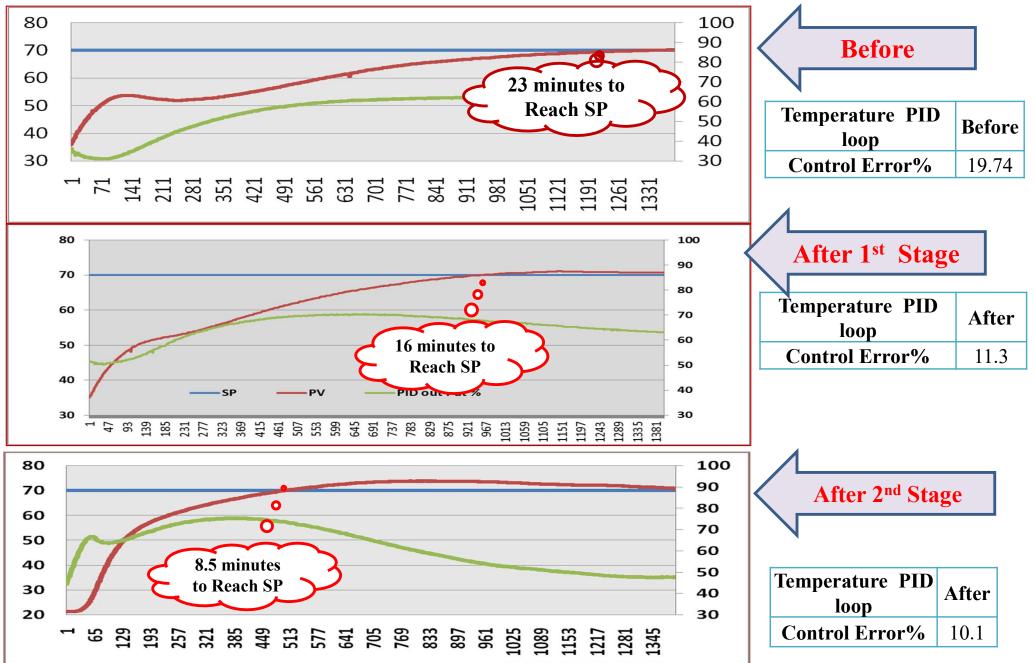
Diagnosis Results: Sluggish Tuning

Suggestion: Increase gain by up to 25%. Observe More for 2nd round improvement.

Loop Name 🕴	Loop Type 🕴	Status 🕴	Diagnosis 🛊	Osc.Status	Var.ldx \$	Avg.Abs%Err \$	CtrLElem.Reversals/hr	Ctrl.Elem.Travel/hr	🕴 Tot.Sat % 🍦 O
LupinGoa_GAC006TIC	Temperature	Low	Sluggish tuning	Non Oscillatory	01067	5,0322	286.9703	138.5275	0
LupinGoa_GAC004TIC	Temperature	Low	Sluggish tuning	Non Oscillatory	0.0762	4,4889	111.2472	69.2539	0



Coating Process : Temperature Set Profile- *(a)* **start up " Stage wise improvement**



Similarly Assessment and Optimisation of "Inlet Hot Air Temperature PID System" done at all 5 Coating Machines using "OPTIMakx" assessment tool.



➢AKXA team with Lupin Team successfully optimized Inlet Hot Air Temperature for the Set points of 25,70/65,55/50 and 80°C for all five coating machine and Observation given for Limitations.

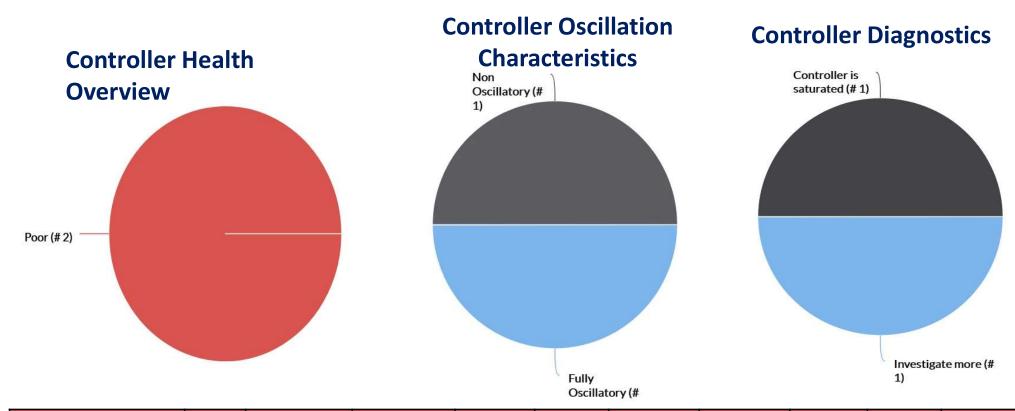
Tablet Coating	Inlet H		emperat int	ure Set	Remarks
Machine	80 °C	70/65° C	55/50° C	25°C	кешагкя
GAC600			\checkmark	\checkmark	Optimized for All Temp Set points
GAC800-900	X	\checkmark	\checkmark	\checkmark	Steam Valve saturation at 80 degree cent - Design capacity
GAC1200			\checkmark	\checkmark	Optimized for All Temp Set points
GAC1500	X	\checkmark	\checkmark	X	Steam Condensate Drain Issue
GAC1700	\checkmark	\checkmark	\checkmark	X	Chilled Water Circulation issue

> Overall Result:

67% reduction in Idle Time (higher machine and labour productivity) + **52% reduction in Steam Wastage** (during the start Up period and also for Re-Starts during Power Failures) + **Quality consistency** as the Set Point is not allowed to deviate for longer time during any unscheduled stoppage.



Ozone and pH OPTIMakx assessment with base case data....



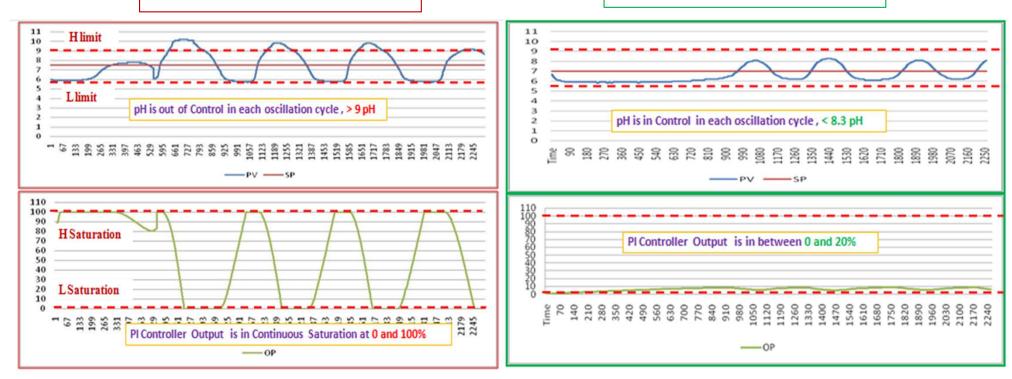
Controller Name	Status	Diagnosis	Osc.Status	Avg.Abs. %.Err	Tot.Sat %	Overshoo t %	Out of Control %		Low.Sat %	P/V.Std. Dev.
LUPINGOA_PWS Ozone	Poor	Controller is saturated	Non- Oscillatory	35	90	209	34	25	65	23.6
LUPINGOA_PWS pH	Poor	Investigate More or Ext. Disrturb.	Fully Oscillatory	17.8	51	36	70	28.	23	1.5



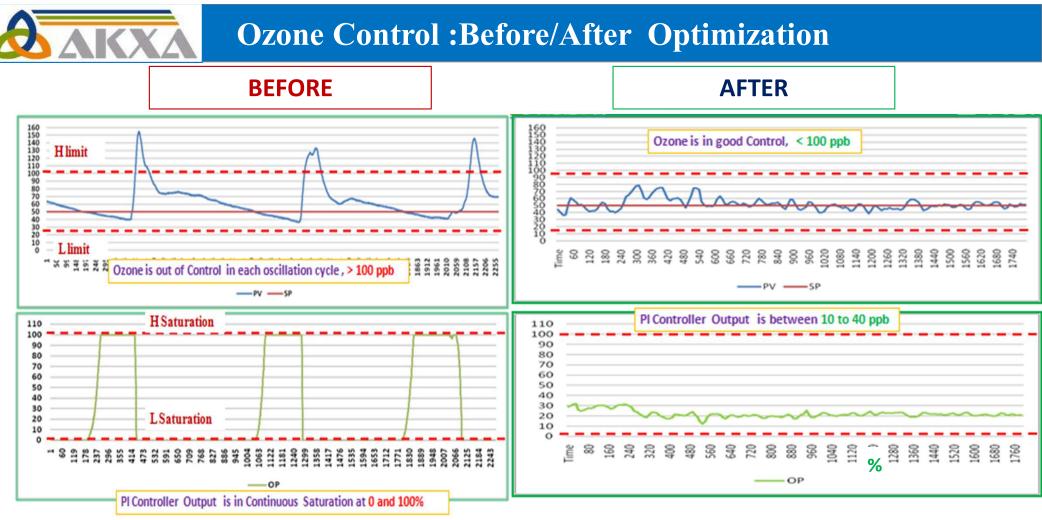
pH Control :Before/After Optimization Results

BEFORE





pH Set point 7		BEFORE	AFTER			
		Base Case	Stage 1 Improvement	Stage 2 Improvement		
	Minimum	5.7	5.8	5.8*		
рН	Maximum	10.2	8.4	8.3		
	Average	7.6	7.3	6.9		
	Diagnosis	External disturbance	Not Applicable	Not Applicable		
Controllor	Avg.Abs.% Control Error	17.8	10.5	10.2		
Controller Performance	Total OP Saturation %	48	0	0		
Indicator	pH Overshoot %	36	12	19		
indicator	Out of Control % (6 to 9 pH)	70	23	0		
	pH Standard Deviation	1.5	0.8	0.8		



		BEFORE	AFTER			
Ozone	Set point 50 ppb	Base Case	Stage 1 Improvement	Stage 2 Improvement		
	Minimum	37	31	36		
OZONE	Maximum	155	78	79		
	Average	64	50	50		
	Diagnosis	Controller saturated	Not Applicable	Not Applicable		
	Avg.Abs.% Control Error	35	16.8	7.4		
Controller	Total OP Saturation %	90	0	0		
Performance Indicator	Ozone Overshoot %	209	56	57		
mulcator	Out of Control % (Range limit 40 to 100 ppb)	34	16	0		
	Ozone Standard Deviation	23.6	10.7	4.8		





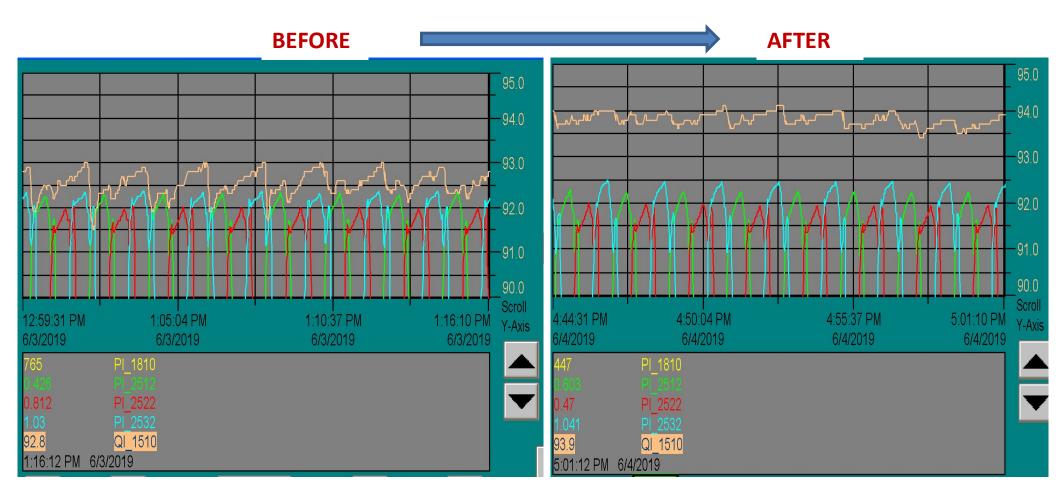
Food Plant Utility Section: Plant Wide Fluctuation Assessment and Root Cause Analysis.

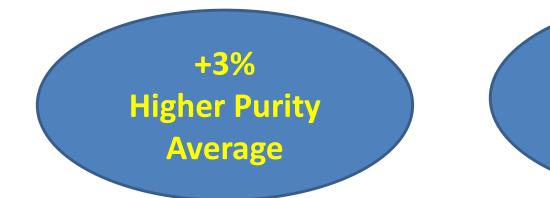
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Oxygen Plant O2 Purity Improvement....

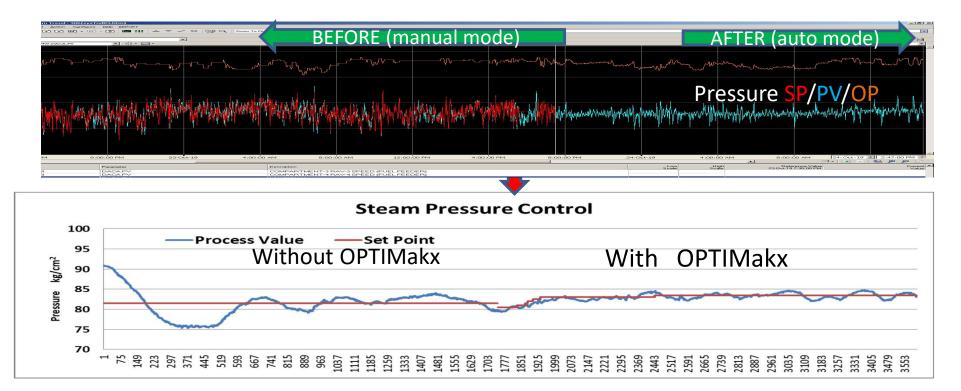




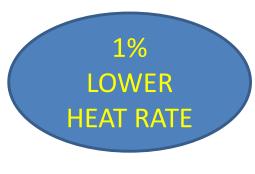


Saving 2,00,000 \$ /yr





Parameter	BEFORE (24 hrs)	AFTER (24 hrs)	
Average Stream Pressure (kg/cm2)	84.8	84.05	
Steam Pressure Std. Dev.	5.2	2.1	
Heat Rate (Kcal/kWH)	3207	3172	

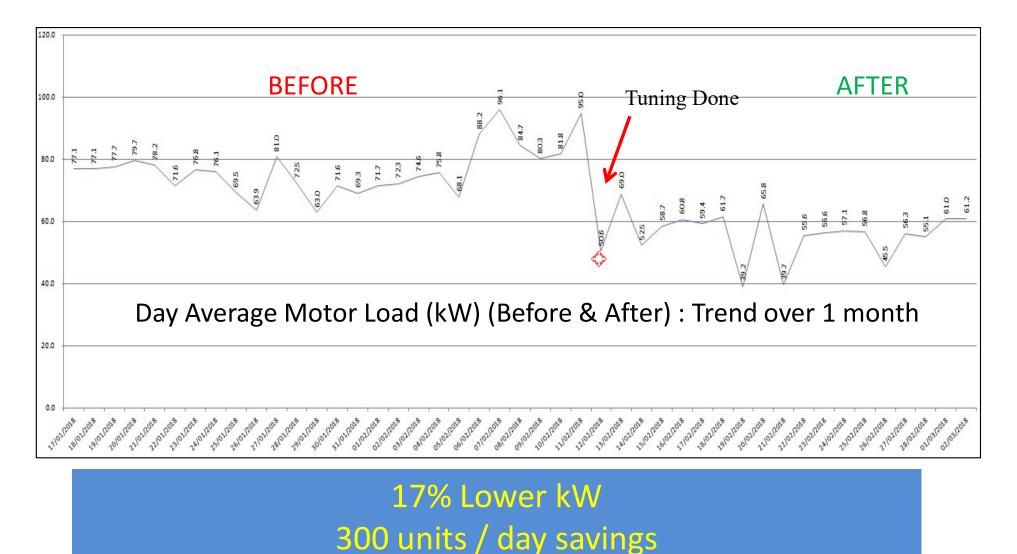




* STEEL PLANT - UTILITY SECTION * (Danfoss VFD panel : Data through RS 485 logger)

>> Issue: RPM saturation at upper limit and Aggressive Response by VFD for load changes

>> ACTION: VFD panel settings for Process Control Module - optimized





TRAINING (on site, customized workshops, offsite at IITs)

AUDIT SERVICES (site visit, benchmarking, scope identification)

ANNUAL CONTRACT (continuous improvement, assured benefits)

SUBSCRIPTION (SAS mode, Remote Access, IoT based Alerts)

PRODUCT (Potable Device, onSite Installation, Corporate Licensing)

CASE SPECIFIC PROJECTS (Troubleshooting, Optimisation, WCM, Industry 4.0, Virtual Sensors, Early Warning Systems, Predictive Models)



Project Execution Stages and Time Line (Total : 8 to 10 Weeks)

KICK OFF MEETING	online / opening meeting with key stake holders	
		START
PRE-AUDIT CHECK	list with plant, facilities, equipment and capacity details	
		1 Week
DATA COLLECTION	customized template, long range/short range data	
		2 Weeks
DATA ANALYSIS	Variability in KPI, PV, Quality, Equipment performances	
		2 Weeks
ASSESSMENT	Gaps, scope for improvement, impact on savings/ROI	
		2 Weeks
REPORTING	Detailed Technical Report, Review Presentations, Action Plan	
		1 Week



MEHER PUDUMJEE

rperson - Energy Efficiency Co Cll - Godrei GBC

Chairman National Award for Excellence In Energy Management 2017

uty Director General ration of Indian Industry

RECOGNITIONS / CLIENT

ESTIMONIALS

Coal mill output has been increased to 16-17 tph against the rated capacity 12-13 tph.

performance of Coal will operation and contributed in imper-

Vicily Vice President (Works) APCL Anjanipuram

ANJANI

APCL is appreciating AAPL team for quick response on APCL request and asso

mine the sector.



We also wish them best of success in their technology Start Up venture

G. Raja Rao **GM** - Instrumentation We also wish this new Tech Start Up company team all the very Best and success in their venture.

Place: YADWAD, Belagavi.

Date : 25th June, 2019

(Technical Head)



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to bring the BENEFITS of INNOVATIVE CONCEPT and ADVANCED TECHNOLOGY to your PROCESS PLANT.."

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